Finned Fuel Element Two-Phase Flow Parameter Measurements Using Real-Time Neutron Radiography*

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Abstract
The measurement of two-phase flow parameters for development of constitutive relationships for the HANARO/MAPLE type finned fuel using Real-Time Neutron Radiography (RTNR) is discussed in this paper. A single element finned Fuel Element Simulator (FES) was used with Freon 134a as the working fluid. To observe the effect of a spacer device on void distribution, single pin tests were performed with and without a spacer present. By analyzing the RTNR images using image processing, the effects of the spacer on the time-averaged and instantaneous void fraction distribution were studied. For the experimental results without a spacer, the time-averaged local void distribution is radially asymmetric and the degree of void fluctuation increases with a decreasing frequency along the heated channel, where the observed asymmetry may be caused by flow induced vibration. For the experimental results with a spacer, the spacer clearly limits any significant vibration and the local void distribution becomes more symmetrical. The spacer however does generate an axial void fraction maximum at the upstream of the spacer with a small depletion zone at the exit of the spacer. By analysis of the instantaneous local void distribution, void fluctuation at the heated wall due to boiling was clearly observed. Also, the agglomeration and breakup of the cold-wall void was evident. The dynamic effects of the local void transients will be discussed in detail.

Key words: Two-Phase Flow, Void Fraction, Neutron Radiography, Finned Fuel Element, Flow Boiling, Spacer Effect

1. Introduction
One advanced technique for real time multi-dimensional void fraction measurement and flow visualization is real-time radiography using either X rays or neutrons. X-ray imaging has been successfully performed for multiphase flows under some conditions but have difficulty penetrating most metals due to the high attenuating power of high atomic number materials due to the large number of electrons present\(^{(1,2,3,4)}\). Real-Time Neutron Radiography (RTNR) is a complementary technique to X-ray radiography that allows for
the measurement of time dependent local void fraction as a function of the spatial r, z, and
temporal t coordinates. Robinson studied neutron radiography using the neutron beam
from the pulse operation TRIGA research reactor\(^5\). Robinson and Wang applied their
neutron radiography techniques to pool boiling phenomena and the movement of steam and
vapour\(^5\). Lindsay et al. observed the stream of oil in a transmission unit for an
automobile\(^6\). Hibiki et al. used neutron radiography to study two-phase flow in narrow
rectangular ducts\(^7\). Sonoda et al. applied a tomographic method to measure the
3-dimensional void fraction using neutron radiography\(^8\). Cimbala et al. used neutron
radiography to visualize streaklines in flow around objects and thus was able to visualize
flow disturbances near the surface\(^9\). Typically, RTNR has less attenuation than X-rays for
metal pipe systems and thus is able to visualize the flow inside experimental apparatus that
simulate real geometries and test conditions\(^10,11,12,13\).

A key limitation for nuclear fuel is critical heat flux (CHF). Researchers have studied
the mechanism of CHF in an attempt to model the physical phenomena\(^14,15\). The main
difficulty in developing an accurate model has been obtaining the information regarding the
phenomena close to the heated wall. Galloway et al. used a photomicrography based
technique to obtain this information\(^16\). Other researchers have studied the effect of heater
length and orientation\(^17\). The general consensus is that CHF is significantly geometry
dependent. As such, CHF can be influenced by geometry effects such as the addition of
fins or spacer elements.

Many heating element designs have in common longitudinal finned elements to
enhance the heat transfer in the fuel assemblies. The element spacers are used to maintain
the gap between the fuel elements\(^18\). At this moment, no comprehensive study has
investigated the effect of a finned element spacer on the time averaged and instantaneous
void distribution in a finned element channel.

Harvel et al.\(^19\) has measured the cross-sectional averaged void fraction in a
single-element flow channel using gamma densitometer and capacitance transducer devices.
However, no spacer was used in the tests and the local void distribution was not observed.
Harvel et al.\(^20\) also conducted capacitance void transducer time dependant void
measurements in air-water flow with MAPLE type fuel elements and significant bundle
effects on the transient behavior of void were observed.

In this research, the time-averaged and instantaneous void distributions were obtained
by processing of the RTNR images from the Freon (134a) boiling experiments for the single
finned element channel.

2. Experimental Apparatus and imaging Method

2.1 RTNR Facility

The RTNR facility used in this work was developed in earlier studies and the
instrumentation is discussed in detail in the references\(^11,21,22\), hence only a summary of the
instrumentation is provided here for completeness.

An LTV Co., model NRTV-2 Real-Time Neutron Radiography camera is used as the
central component of the RTNR system\(^21\). The other components in the system include a
time code generator (Telcom Research Model T5010), a Mitsubishi video cassette recorder
(VHS and S-VHS), an image processing board (Data Translation DT2853,
DT2861,DT3152), and a personal computer (Pentium II, HLI++ image software).

The RTNR camera generates a standard RS-330 video signal to a VCR for video
storage at a sample rate of 30 frames/second. The video can then be acquired by the image
processing board for enhancement and analysis by computer.
1. R134a outlet temperature  2. R134a outlet pressure   3. Bypass valve  

Fig 1: Single pin test loop

The RTNR camera operates under relatively low thermal neutron fluxes (on the order from $10^7 - 10^8 n/(cm^2-s)$). The spatial resolution of the RTNR camera is approximately 1 mm for a high contrast image for a region of 20.0 cm x 20.0 cm. The temporal resolution of the system is limited by the sampling rate of 30 frames/s or 33.0 ms (16.5 ms per field). The exposure time for each image is also 33.0 ms as the camera uses a continuous exposure feature.

The Real-Time Neutron Radiography system is used in the neutron radiography facility at the McMaster Nuclear Reactor (MNR). The neutron flux for the MNR neutron radiography facility is approximately $10^8 n/(cm^2-s)$ when the reactor is operated at 2.0 MWth power.

2.2 Single Element Experimental Apparatus and Instruments

To observe the effect of spacers on the void distribution, two sets of tests were performed; first set was performed by using a test section having three spacers and the second was done by using a test section without spacers. The test loop for the finned fuel element simulator is shown in Fig. 1. The element is heated by the hot water flowing through the inside of the finned element. The finned element was inserted into a 15.75 mm ID Aluminium tube. The temperatures of the Freon side and the water side were measured by type-T thermocouples. The water flow rate was measured by a turbine flow meter and the Freon flow was measured by a venturi meter. The system pressure was measured by a pressure transducer.
2.3 Image Analyses and Void Determination

The procedure for the image analyses and determination of the void fraction are as follows(23):

a) A look-up table (LUT) for image capture using HLI++ was determined in such a way to maximize the dynamic range of the output grey level. The wider the dynamic range is, the less the void calculation error is. The LUT for this study is such that the input grey level between 0 to 130 is expanded to the allowable grey level between 0 and 255.

b) The Sobel technique was applied to obtain the object edge and to obtain the degree of rotation of the image which will make the image of the test section exactly vertical.

c) To remove the target integration effect(12), a shading correction function is applied.

d) The calibration constant is found to determine the dependency of the corrected grey level on the liquid path length.

e) By using the calibration curve, and the full image and the two-phase image, the lateral void fraction distribution is obtained.

f) From the lateral void fraction distribution, the cross-sectional averaged void fraction and the local void distribution are obtained.

The pixel intensity for any image can be represented by the following equation:

\[ I(x, y, z) = I_o B e^{(-\beta_f \sum f x_f)} e^{(-\beta_w \sum w x_w)} \]  

(1)

where \( I_f \) represents the grey level of a pixel for the full image, \( I_o \) is the unperturbed Grey level, B is the buildup factor, \( \beta_f \) and \( \beta_w \) are the calibration coefficient and \( \sum f \) and \( \sum w \) are the macroscopic cross-section for Freon and water respectively. \( X_f \) and \( X_w \) are the liquid Freon path length and the water path length. \( X_{f\text{max}} \) and \( X_{w\text{max}} \) are the path lengths for a full test section, i.e. no void fraction.

As the water path length is fixed, \( X_w \) is equal to \( X_{w\text{max}} \) in any pixel. Thus, Eq. 1 can be used to determine the line-averaged void fraction which can be expressed by the following equation:

\[ \alpha(y, z) = 1 - \frac{x_f}{x_{f\text{max}}} = \frac{1}{\beta \sum f x_{f\text{max}}} \ln\left(\frac{I_f}{I_o}\right) \]  

(2)

The lateral void fraction does not truly represent the type of void migration under consideration as length averaging is inherent. However, weighting the void fraction with the Freon path length provides a cross-sectional averaged void fraction at each axial location(24). The result of the cross-sectional averaged void fraction is given by the following Equation:

\[ \overline{\alpha}(z) = \frac{\int_0^y \alpha(y, z)L(y)dy}{\int_0^y L(y)dy} \]  

(3)

where \( L(y) \) is the beam path length.

The above expressions can be evaluated for each image and pixel. As such, each calculated value represents an instantaneous measurement corresponding to 33 ms or 30
frames per second. By accounting for the beam path length and integrating across a given cross section using equation 3, we can obtain an instantaneous cross-sectional averaged void fraction.

Time averaging results can be achieved by averaging the results of successive images. While time averaging loses the instantaneous result, it provides additional insight into the phenomena under study because there is a reduction in error caused by neutron noise which tends to average out of the results.

The local instantaneous void distribution was determined by using Mudde’s technique\(^{(25)}\). In Mudde’s technique, the void is assumed to be symmetrical and each pixel represents successive layers around the centre. This technique works reasonably well for concentric geometries such as pipes and annuli. The void fraction is calculated for the outer layers first as information on the void in just the outer layer can be obtained from pixels near the outer wall. As the calculation proceeds to the inner radii, the values are corrected with the values previously calculated. Essentially, the measured void fraction for the next ring in represents a path length averaging of that ring plus the outer ring. Since the void fraction has already been determined for the outer ring, it is possible to calculate the void fraction for each subsequent ring.

3. Experimental Results

3.1 Test Matrices and Process Data Analysis

Experiments are performed using Freon 134a as the working fluid. The mass flux is varied from 37 to 110 kg/m\(^2\)s. The inlet subcooling is maintained at approximately 10°C and the heat flux is maintained at approximately 120 kW/m\(^2\). The system pressure is maintained at approximately 640 kPa(a).

3.2 RTNR Image

In Fig. 2, RTNR processed images for the case with and without a spacer at 50 kg/m\(^2\)s of Freon mass flux is shown. The processed image was made by the subtraction of the full image from the two-phase image as discussed above. In the processed images for these figures, the darker region represents the higher void region. In Fig. 2, the spacer is easily observed. It is also observed that the void fraction has a maximum near the upstream of the spacer.

3.3 Time and Cross-sectional Averaged Void Fraction Distribution

The time and cross-sectional averaged axial void fraction distributions for Freon mass fluxes ranging from 50 to 110 kg/m\(^2\)s were studied. A typical result with and without spacer for the higher mass flux is shown in Fig. 3.

For low mass fluxes without the presence of a spacer, the time averaged axial void fraction increases slightly with increasing elevation. With the spacer present, the averaged axial void fraction is no longer axially uniform with significant void fraction peaks before and after the spacer.

Typically, for Freon mass fluxes below 90 kg/m\(^2\)s, the void fraction peak occurs just before the spacer. Above 90 kg/m\(^2\)s, the void fraction peak occurs on either side of the spacer. It is surmised that the larger momentum component of the flow is now strong enough to push the void past the spacer.

Fig. 4 shows the observed axial gradients in the time and cross-sectional averaged void fraction for cases both with and without a spacer and for mass fluxes of 50 kg/m\(^2\)s and 110 kg/m\(^2\)s. Note that regardless of mass flux, the void gradients are the same when no spacer is present. However, when a spacer is present, the void gradient is no longer constant.
Fig. 2: 50 kg/m²s (a) without spacer, (b) with spacer. Dark colour corresponds to high void. Bright colour corresponds to low void.

Fig. 3: Time averaged axial void fraction for 110 kg/m²s both with and without a spacer.

Fig. 4: A comparison of the void gradient at 50 and 110 kg/m²s for both with and without a spacer.
Hence, the presence of the spacer significantly affects the acceleration component of the two-phase flow. The disturbance after the spacer is expected to decrease as the flow re-develops after the presence of the spacer.

Another observation is that the presence of the first and second spacers at 0 cm and 29 cm in the channel did not introduce such disturbances in the flow. The probable cause of the lack of influence by the first and second spacers is likely due to a lower void fraction and a more homogeneous flow distribution. By the time the third spacer is approached, a significant amount of void has been generated and the flow is likely non-homogeneous.

Figure 5(a) show the local void fraction for the case without a spacer and a Freon mass flux of 110 kg/m²s. The majority of the local void fraction is distributed with a range of 0.2 to 0.4. The void is evenly distributed with a slight tendency towards the left side of the channel. This is likely due to the fact that the channel and the fuel element simulator cannot be perfectly vertical and hence the buoyancy force is slightly off the axial direction.

Figure 5(b) shows the time averaged local void fraction distributions for the case with a spacer and a Freon mass Flux of 110 kg/m²s. Note that also due to slight variances in process boundary conditions (heat flux, pressure, inlet subcooling) that this case has a slightly higher heat content than does the similar case shown in Fig. 5(a) without a spacer. Hence, not only is a spacer present but slightly more void is present as well.

Figure 5(b) shows that the local void fraction distribution below the spacer is quite uniform in the range of 0.12 to 0.4 and is thus very similar to the same situation without a spacer. However, above the spacer, the local void fraction has increased significantly due to two factors. One is the extra heat addition. The second is that the spacer has introduced a region where void fraction can be trapped.

Note that the results observed in Fig. 5(a) are typical for the case without spacers for all tests at different Freon mass fluxes. Essentially, as the mass flux decreases, the average void fraction increases as expected but the flow remains uniform and homogeneous. This observation is expected to break down once the mass flux is small enough such that the void fraction is large enough to form slug flow or churn flow. At the lowest flow rate tested, there is some indication that the flow regime has indeed changed and the local void distribution is becoming non-homogeneous even when time averaged.

In the case where a spacer is present, the homogeneous behaviour is also observed similar to that for the cases without a spacer. In addition, the local void begins to collect before the spacer. More and more void becomes trapped before the spacer as the Freon mass flux decreases. Since the channel is vertical, the spacer is effectively acting as a flow blockage and the higher momentum liquid is passing through the spacer and the lower momentum void is being trapped. As mass flux, and hence momentum increases, the Freon liquid acts similar to a ram and pushes the fluid through the spacer.

Figure 5(c) supports this hypothesis by showing a void peak before the spacer at a slightly lower mass flux (95 kg/m²s) than for Fig. 5(b).

The point where the flow becomes able to push the vapour through the spacer is not entirely clear and more experiments are required. Also, it is expected that this behaviour will change significantly based upon the type of upstream flow regime. Non-homogeneous flow regimes are expected to provide greater turbulence and thus have different behaviour.

### 3.4 Instantaneous Void Fraction

Instantaneous void fraction distributions were analyzed for all cases. First, visual observations indicated that for the lower Freon mass fluxes, slug flow was indeed present as Gouse and Hwang\(^{(26)}\) suggested. Analysis of the instantaneous void distributions support
the visual observations. Also, the quantitative analysis further shows that at higher axial locations, the amount of fluctuation increases and the fluctuation frequency decreases. This indicates that the vapor bubble size is increasing due to additional vapour generation and agglomeration.

Calculations of instantaneous void distributions at higher Freon mass fluxes (110 kg/m²s) do not show slug flow, but instead indicate a more bubbly flow or homogeneous pattern supporting the observations made from the time averaged void distribution analysis.

The time-dependent fluctuation of void fraction at several locations along the channel. At Z=37 cm, the mid-point between the second spacer and the third spacer, the void wave shape is very similar to that for without a spacer. However, at Z=44 cm, just below the spacer, the fluctuation amplitude increases and is larger than the fluctuation for without a spacer. The void wave at Z=49 cm is similar to that at Z=37 cm, which means the spacer effect almost disappears at this location.

Fig. 5: Time averaged local void fraction distributions of boiling Freon in a vertical annulus where Blue is low void and Red is high void. 4.5 cm radius is the heated wall and 8.0 cm is the outer wall of the annulus: (a) mass flux of 110 kg/m²s without a spacer, (b) mass flux of 110 kg/m²s with a spacer, (c) mass flux of 95 kg/m²s with a spacer.

The instantaneous local void fraction distributions show where the fluctuation of void at the heated wall was due to boiling. Also, the propagation of the void wave, the agglomeration, and breakup of the wall void are also observed.

An instantaneous cross sectional averaged void fraction trace is shown in Fig. 6 for a mass flux of 50 kg/m²s without a spacer. The measurements are taken at 37 cm and 44 cm. The traces indicate that the average void fraction is higher at 44 cm as expected. The two traces can be correlated to determine the velocity of the void fraction peaks.

Using the instantaneous cross-sectional averaged void fraction results, it is possible to identify the centroid of a void as it passes a certain elevation. This same void packet will eventually arrive at a higher elevation and the time that the centroid of the void passes this location can be measured. This provides information related to the vapor phase velocity. Note that variances in the vapor phase velocity are expected since the measurements may indicate a void packet and not necessarily a single bubble. Thus, it is possible that the void packet is accelerating or decelerating due to different bubble shapes and sizes.
The velocity of the vapour phase is determined in a range of 10.1 cm/s to 12.7 cm/s. The data suggests that each successive void packet is accelerating. The results also suggest that the void packets have a tendency to change in magnitude. Review of the images indicate that some of the changes are due to agglomeration while others are due to a break up of the packet.

Similar instantaneous cross sectional averaged void fraction traces are shown in Fig. 7 for a mass flux of 50 kg/m²-s but for the case where the spacer is included. The measurements are taken at 37 cm, 44 cm, 46 cm, and 49 cm from the inlet of the test section. 44 cm is just before the spacer and 46 cm is just after the spacer. At 37 cm, the mid-point between the second spacer and the third spacer, the void wave shape is very similar to that for without a spacer. However, at Z=44 cm, just below the spacer, the fluctuation amplitude increases and is larger than the fluctuation for without a spacer. The void wave at Z=49 cm is similar to that at Z=37 cm, which means the spacer effect almost disappears at this location. The results indicate that the vapor velocity before the space is approximately 7 cm/s before the spacer and approximately 6 cm/s after the spacer. However, across the spacer, the vapor velocity appears to reduce to approximately 2.9 cm/s which correlates to the spacer trapping the void in place and disturbing the flow. Review of the video images supports vapor trapping to occur at the spacer under a mass flux of 50 kg/m²-s.

Void trapping is further supported by the instantaneous void fraction distributions shown in Fig. 8. These images are produced by employing Mudde’s technique to capture the instantaneous void fraction bout axially and radially although significant noise can exist in the images due to statistical fluctuations in the neutron beam. In this case, the void fraction can be seen moving up the flow channel and collecting both just before and after the spacer. Fig. 8 also shows that the void formation along the heated surface is evident and then transports downstream in large packets. Due to the orifice type restriction by the spacer, the shape of the void is flatter and the interface is more wavy than further upstream. This may be due to agglomeration of void from nucleation sites. The spacer effects also can be clearly shown near the outer side tube where void is clearly trapped and collapses after accumulation to certain size. Similar void trapping also can be observed on the downstream side of the spacer near the tube wall.
Fig. 8: Instantaneous Local Void Fraction Distribution with a spacer, $G=50 \text{ kg/m}^2\text{s}$
4. Conclusion

From the image analysis of the RTNR test for the single-element flow channel subcooled flow boiling with and without spacers, the followings conclusions were drawn:

a) The cross sectional averaged void fraction axial profiles decreases with increasing Freon mass flux.

b) The spacer generates an axial void fraction maximum at the upstream of the spacer. The degree of these peaks is higher for the lower mass fluxes. At higher mass fluxes, the void fraction peaks after the spacer.

c) The spacer limits any FES vibration and local void distribution becomes more radially symmetric.

d) For the test without spacer, the time-averaged local void distribution becomes radially asymmetric. It may be due to the flow induced vibration of the FES.

e) For the case without spacer, the degree of the void fluctuation increases along the heated channel. However, the fluctuation frequency decreases along the heated channel.

f) For the case with spacer, the degree of void fluctuation is largest at the upstream of the spacer.

g) The magnitude of void fluctuation decreases as the Freon mass flux increases largely due to the homogeneity of the flow.

h) From the analysis of the instantaneous local void fraction distribution, the fluctuation of void at the heated wall due to the boiling was clearly observed. Also, the agglomeration and breakup of the cold-wall void was evident.

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